

This is a Rayleigh-Taylor instability problem with thermal conduction. The data files are:

Density

Pressure

V_x

V_y

All these quantities are given as a function of X and Y. The gravity is oriented in the negative-Y direction. X is the horizontal direction, Y is vertical.

In the data files, all the quantities are in SI units (rho in kg/m³, P in N/m², V in m/s).

There are also files with plots of :

Density (in g/cc) profile along Y

Temperature (in KeV) profile along Y

Pressure (in Megabar) profile along Y

There are also contour plots of :

Density (in g/cc) in X-Y

Vorticity (in 1/nanosecond) in XY

The gravitational acceleration is:

g= -1e14 m/s² (directed in the negative y-direction)

The thermal diffusion is included through:

$$\rho c_v \left(\frac{\partial T}{\partial t} + \mathbf{v} \cdot \nabla T \right) = -p \nabla \cdot \mathbf{v} + \nabla \cdot \kappa_0 T^{2.5} \nabla T$$

I use SI units but the temperature is in Joules.

Here $\kappa_0 = 3.734e+69$, $c_v = 7.186e+26$, the

temperature T is in Joules, rho in kg/m³, P in N/m² and V in m/s.

The adiabatic index is $\gamma = 5/3$ (I don't think you need that)

The equation of state is

P=4.7904e+26 ρ T

where the Temperature is in Joules, rho in kg/m³ and P in N/m².

Boundary Conditions:

(a) Reflective BC in X

(b) At the bottom (Y=0), the heat flux is assigned

$$q = -\kappa_0 T^{2.5} \nabla T \big|_{y=0} = 5.876e18 \text{ W/m}^2$$

(c) At the top, the heat flux = 0.

(d) For the other hydro variables the BCs are Outflow at the bottom (Y=0) and inflow at the top. It should not matter much what you use. Below is what I use (it seems to work).

! boundary conditions on the bottom boundary

$$v(i,0) = v(i,4) - 2*(v(i,3) - v(i,1))$$

$$\rho(i,0) = \rho(i,1)*v(i,1)/v(i,0)$$

$$u(i,0) = u(i,1)$$

$$p(i,0) = p(i,1) - 0.5*(\rho(i,0) + \rho(i,1))*\text{acceleration}*dy + \rho(i,1)*v(i,1)**2 - \rho(i,0)*v(i,0)**2$$

The first is the continuity of the second derivative

The second is the continuity of the normal mass flow

The third is the continuity of the tangential flow

The fourth is the total pressure equilibrium (here $g < 0$)

$$\frac{d(P + \rho v^2)}{dy} = \rho g$$

! boundary conditions on the top boundary

$$u(i,ny+1) = u(i,ny)$$

$$v(i,ny+1) = v(i,ny)$$

$$rsh = 1.66667$$

$$\text{del_hat} = \text{acceleration} * \rho(i,ny) / p(i,ny) * (rsh - 1.) / rsh$$

$$p(i,ny+1) = p(i,ny) * \text{dexp}((\text{del_hat} * dy - \text{del_hat}**2 * dy**2 * 0.5) * rsh / (rsh - 1.))$$

$$\rho(i,ny+1) = \rho(i,ny) * \text{dexp}((\text{del_hat} * dy - \text{del_hat}**2 * dy**2 * 0.5) / (rsh - 1.))$$

Here I am using the equilibrium again $\frac{d(P)}{dy} = \rho g$ without flow and the

isentropic condition $p = \text{const } \rho^{1.667}$. The exponentials are used to avoid negative pressures and densities.