

Solutions Problem Set 2

1) From the ideal gas law

$$pV = Nk_B T$$

we have for an isotherm, i.e. T held constant

$$pV = \text{const} \Rightarrow \boxed{p \sim \frac{1}{V} \text{ on an isotherm}}$$

For an adiabat, i.e. S held const, we use from Problem (1)

$$E(S, V, N) = E_0 \left(\frac{V}{V_0} \right)^{-2/3} \left(\frac{N}{N_0} \right)^{5/3} \exp \left[\frac{2}{3} \left(\frac{S}{N} - \frac{S_0}{N_0} \right) / k_B \right]$$

$$p = - \left(\frac{\partial E}{\partial V} \right)_{S, N} = \frac{2}{3} E_0 V_0 \left(\frac{V}{V_0} \right)^{-5/3} \left(\frac{N}{N_0} \right)^{5/3} \exp \left[\frac{2}{3} \left(\frac{S}{N} - \frac{S_0}{N_0} \right) / k_B \right]$$

so when S and N are held const

$$p V^{5/3} = \text{const} \Rightarrow \boxed{p \sim \frac{1}{V^{5/3}} \text{ on an adiabat}}$$

or $V \sim \frac{1}{p}$ on an isotherm (const T)

$V \sim \frac{1}{p^{3/5}}$ on an adiabat (const S)

2)

Prove $\left(\frac{\partial C_p}{\partial p}\right)_T = -TV \left[\alpha^2 + \left(\frac{\partial \alpha}{\partial T}\right)_p\right]$

$$C_p = T \left(\frac{\partial S}{\partial T}\right)_p = \text{definition of } C_p$$

$$S(T, p) = -\left(\frac{\partial G(T, p)}{\partial T}\right)_p$$

$$C_p = -T \left(\frac{\partial^2 G}{\partial T^2}\right)_p$$

$$\left(\frac{\partial C_p}{\partial p}\right)_T = -T \left(\frac{\partial^3 G}{\partial T^2 \partial p}\right) = -T \left(\frac{\partial^2}{\partial T^2} \left(\frac{\partial G}{\partial p}\right)_T\right)_p$$

$$= -T \left(\frac{\partial^2 V}{\partial T^2}\right)_p = -T \left(\frac{\partial}{\partial T} \left(\frac{\partial V}{\partial T}\right)_p\right)_p$$

$$= -T \frac{\partial}{\partial T} (V\alpha)_p \quad - \text{using definition of } \alpha$$

$$= -TV \left(\frac{\partial \alpha}{\partial T}\right)_p - T\alpha \left(\frac{\partial V}{\partial T}\right)_p$$

$$= -TV \left(\frac{\partial \alpha}{\partial T}\right)_p - T\alpha V\alpha$$

$$\boxed{\left(\frac{\partial C_p}{\partial p}\right)_T = -TV \left[\alpha^2 + \left(\frac{\partial \alpha}{\partial T}\right)_p\right]}$$

3) $T = \left(\frac{V}{V_0}\right)^\gamma T_0$ gives temperature as system changes volume V

a) work done on the gas

$$dW = -p dV$$

use ideal gas $pV = Nk_B T \Rightarrow p = \frac{Nk_B T}{V}$

$$dW = -Nk_B T \frac{dV}{V}$$

total work done is

$$\begin{aligned} W &= \int dW = -Nk_B \int_{V_0}^{V_1} \frac{dV}{V} T(V) \\ &= Nk_B \int_{V_0}^{V_1} \frac{dV}{V} \left(\frac{V}{V_0}\right)^\gamma T_0 = -Nk_B T_0 \int_{V_0}^{V_1} dV \frac{V^{\gamma-1}}{V_0^\gamma} \\ &= \frac{-Nk_B T_0}{V_0^\gamma} \frac{V_1^\gamma - V_0^\gamma}{\gamma} = \frac{Nk_B T_0}{\gamma} \left[1 - \left(\frac{V_1}{V_0}\right)^\gamma\right] \end{aligned}$$

$$W = \frac{Nk_B T_0}{\gamma} \left[1 - \left(\frac{V_1}{V_0}\right)^\gamma\right]$$

b) use $E = \frac{3}{2} Nk_B T$ for ideal gas

$$\Delta E = \frac{3}{2} Nk_B (T_1 - T_0) = \frac{3}{2} Nk_B T_0 \left[\left(\frac{V_1}{V_0}\right)^\gamma - 1\right]$$

c) Heat transfer to the gas

$$\begin{aligned} dQ &\equiv T dS = dE - dW && \text{(from } dE = T dS - p dV) \\ \Rightarrow \Delta Q &= \Delta E - \Delta W && \text{and } dW = -p dV \\ \Delta Q &= N k_B T_0 \left[\left(\frac{V_1}{V_0} \right)^\gamma - 1 \right] \frac{3}{2} - \frac{N k_B T_0}{\gamma} \left[1 - \left(\frac{V_1}{V_0} \right)^\gamma \right] \end{aligned}$$

$$\Delta Q = N k_B T_0 \left[\left(\frac{V_1}{V_0} \right)^\gamma - 1 \right] \left[\frac{3}{2} + \frac{1}{\gamma} \right]$$

$$\Delta Q = 0 \text{ when } \frac{3}{2} + \frac{1}{\gamma} = 0 \Rightarrow \boxed{\gamma = -\frac{2}{3}}$$

From problem ① if the gas expands adiabatically
(i.e. $\Delta S = 0 \Rightarrow \Delta Q = 0$) then
 $p V^{5/3} = \text{const}$

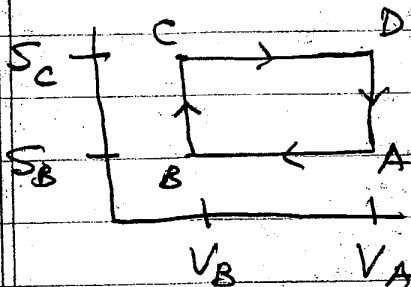
using $pV = N k_B T$ the above becomes

$$\frac{N k_B T}{V} V^{5/3} = N k_B T V^{2/3} = \text{const}$$

$$\text{or } T \sim V^{-2/3}$$

which gives $\gamma = -2/3$ in
agreement with part (c)

4) Otto cycle



heat extracted in $B \rightarrow C$

work done by system in $C \rightarrow D$

heat returned in $D \rightarrow A$

work done on system in $A \rightarrow B$

$$\text{efficiency } \epsilon \equiv \frac{Q_{BC} - Q_{AD}}{Q_{BC}} = 1 - \frac{Q_{AD}}{Q_{BC}}$$

using $dQ = TdS$, the heat extracted from reservoir and added to the system in step $B \rightarrow C$

$$Q_{BC} = \int_B^C T dS \quad \text{integral is taken at constant } V$$

$$\text{Now we know } T = \left(\frac{\partial E}{\partial S} \right)_{V, N} \quad \text{so}$$

$$Q_{BC} = \int_B^C \left(\frac{\partial E}{\partial S} \right)_{V, N} dS = E_C - E_B$$

(we can do the integral since trajectory of integration is at constant V , or more generally,

$$TdS = dE + PdV, \text{ but here } dV = 0)$$

For ideal gas, as assumed here, $E = \frac{3}{2} N k_B T$

So $Q_{BC} = \frac{3}{2} N k_B (T_C - T_B)$

similarly

$Q_{AD} = \frac{3}{2} N k_B (T_D - T_A)$

efficiency

$\epsilon = 1 - \frac{(T_D - T_A)}{(T_C - T_B)}$

Finally we need to relate T_A, T_B, T_C, T_D to the volumes V_A and V_B

From problem (1) we have for the adiabatic expansion of the ideal gas,

$p V^{5/3} = \text{const}$

using $p V = N k_B T$ gives $N k_B T V^{2/3} = \text{const}$

So along path $C \rightarrow D$ we get

$T_C V_B^{2/3} = T_D V_A^{2/3} \Rightarrow T_D = T_C \left(\frac{V_B}{V_A} \right)^{2/3}$

and along path $B \rightarrow A$ we get

$T_B V_B^{2/3} = T_A V_A^{2/3} \Rightarrow T_A = T_B \left(\frac{V_B}{V_A} \right)^{2/3}$

So

$$\epsilon = 1 - \frac{\left[T_C \left(\frac{V_B}{V_A} \right)^{2/3} - T_B \left(\frac{V_B}{V_A} \right)^{2/3} \right]}{T_C - T_B}$$

$$\epsilon = 1 - \left(\frac{V_B}{V_A} \right)^{2/3}$$

Now for ideal gas

$$C_V = \frac{3}{2} N k_B$$

$$C_P = \frac{5}{2} N k_B$$

$$\frac{C_P - C_V}{C_V} = \frac{5-3}{3} = \frac{2}{3}$$

$$\epsilon = 1 - \left(\frac{V_B}{V_A} \right)^{\gamma} \quad \gamma = (C_P - C_V)/C_V$$